

Amendment to the Claims:

1. (Previously Presented) A process to prepare base oils from a Fischer-Tropsch synthesis product, the processing comprising
 - (a) separating the Fischer-Tropsch synthesis product into a fraction (i) boiling in the middle distillate range and below, a heavy ends fraction (iii) and an intermediate base oil precursor fraction (ii) boiling between fraction (i) and fraction (iii);
 - (b) subjecting the base oil precursor fraction (ii) to a catalytic hydroisomerization and catalytic dewaxing process to yield one or more base oil grades;
 - (c) subjecting the heavy ends fraction (iii) to a conversion step to yield a fraction (iv) boiling below the heavy ends fraction (iii); and,
 - (d) subjecting the high boiling fraction (v) of fraction (iv) to a catalytic hydroisomerization and catalytic dewaxing process to yield one or more base oil grades.
2. (Previously Presented) The process of according to claim 1, wherein the heavy ends fraction (iii) has an initial boiling point of between 500 °C and 600 °C.
3. (Previously Presented) The process of claim 1, wherein step (b) is performed in the presence of a catalyst comprising a noble metal hydrogenation component and a molecular sieve selected from the group consisting of zeolite beta, ZSM-23, ZSM-22, ZSM-35 or ZSM-12.
4. (Withdrawn) The process of claim 1, wherein step (c) comprises a hydrocracking/hydroisomerization process comprising contacting the heavy ends fraction (iii) with an amorphous catalyst comprising an acidic functionality and a hydrogenation/dehydrogenation functionality.
5. (Withdrawn) The process of claim 1, wherein step (c) is performed under catalytic dewaxing conditions in the presence of a catalyst comprising a molecular sieve having a 12 member ring structure and a metal hydrogenation components.

6. (Withdrawn) The process of claim 5, wherein step (c) and (d) take place simultaneously.
7. (Previously Presented) The process of claim 1, wherein step (d) is performed in the presence of a catalyst comprising a noble metal hydrogenation component and a molecular sieve selected from the group of zeolite beta, ZSM-23, ZSM-22, ZSM-35 or ZSM-12.
8. (Previously Presented) The process of claim 1, wherein the feed to step (a), step (b) and/or step (c) is first hydrogenated.
9. (Previously Presented) The process of claim 1, wherein step (c) comprises a thermal cracking process.
10. (Withdrawn) The process of claim 1, wherein step (c) comprises a catalytic cracking process.
11. (Previously Presented) The process of claim 9, wherein the fraction boiling below 370 °C as obtained in step (c) is subjected to an oligomerization step (f).
12. (Previously Presented) The process of claim 11, wherein a base oil fraction is prepared in step (f) and which base oil fraction is mixed with the base oil products obtained in step (b) and/or (d).
13. (Previously Presented) The process of claim 11, wherein a base oil fraction is prepared in step (f) and which base oil fraction is dewaxed in step (b).
14. (Previously Presented) The process of claim 1, wherein the effluent of step (c) is provided to step (a), such that in effect steps (b) and (d) take place simultaneously.

Claim 15 (Canceled).

16. (Previously Presented) The process of claim 2, wherein step (b) is performed in the presence of a catalyst comprising a noble metal hydrogenation component and a molecular sieve selected from the group consisting of zeolite beta, ZSM-23, ZSM-22, ZSM-35 or ZSM-12.

17. (Withdrawn) The process of claim 2, wherein step (c) comprises a hydrocracking/hydroisomerization process comprising contacting the heavy ends fraction (iii) with an amorphous catalyst comprising an acidic functionality and a hydrogenation/dehydrogenation functionality.

18. (Withdrawn) The process of claim 2, step (c) is performed under catalytic dewaxing conditions in the presence of a catalyst comprising a molecular sieve having a 12 member ring structure and a metal hydrogenation component.

19. (Withdrawn) The process of claim 18, wherein step (c) and (d) take place simultaneously.

20. (Previously Presented) The process of claim 2, wherein step (d) is performed in the presence of a catalyst comprising a noble metal hydrogenation component and a molecular sieve selected from the group of zeolite beta, ZSM-23, ZSM-22, ZSM-35 or ZSM-12.

21. (Previously Presented) The process of claim 2, wherein the feed to step (a), step (b) and/or step (c) is first hydrogenated.

22. (Previously Presented) The process of claim 2, wherein step (c) comprises a thermal cracking process.

23. (Withdrawn) The process of claim 2, wherein step (c) comprises a catalytic cracking process.

24. (Withdrawn) The process of claim 23, wherein the fraction boiling below 370 °C as obtained in step (c) is subjected to an oligomerization step (f).

25. (Withdrawn) The process of claim 24, wherein a base oil fraction is prepared in step (f) and which base oil fraction is mixed with the base oil products obtained in step (b) and/or (d).

26. (Withdrawn) The process of claim 24, wherein a base oil fraction is prepared in step (f) and which base oil fraction is dewaxed in step (b).

27. (Withdrawn) The process of claim 2, wherein the effluent of step (c) is provided to step (a), such that in effect steps (b) and (d) take place simultaneously.

28. (Withdrawn) The process of claim 10, wherein the fraction boiling below 370 °C as obtained in step (c) is subjected to an oligomerization step (f).